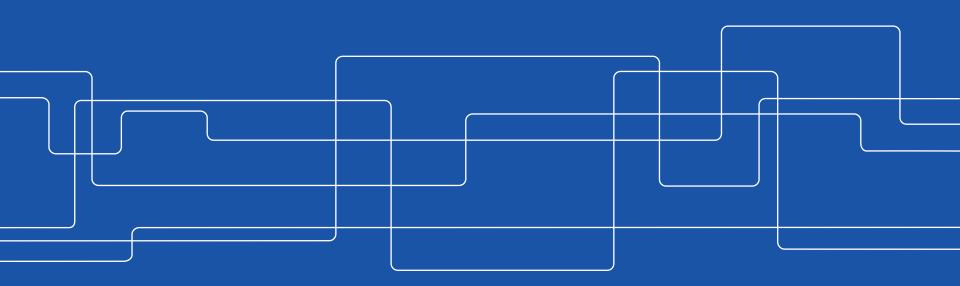


TRANSESTERIFICATION OF RAPESEED OIL BY SOLID OXIDE CATALYSTS JERRY LUIS SOLIS VALDIVIA PHD STUDENT

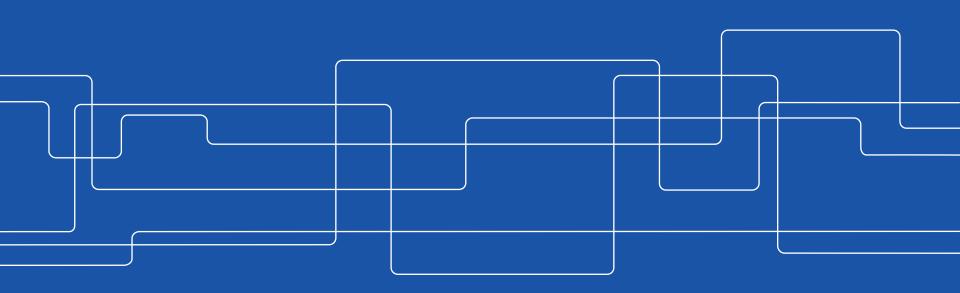
POKE – SUMMER SCHOOL SAAREMAA, ESTONIA – 2014





OUTLINE

- > INTRODUCTION
- BACKGROUND
- EXPERIMENTAL METHOD
- ➢ RESULTS AND DISCUSSION
- > CONCLUSIONS
- FURTHER STUDIES



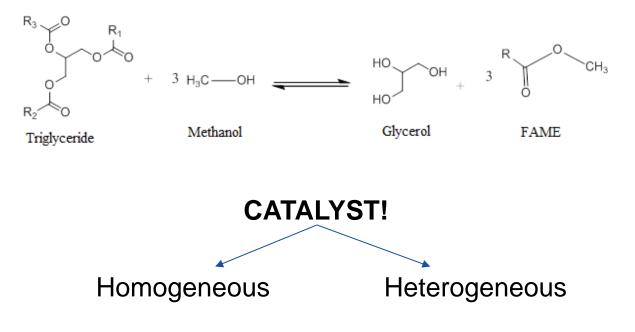


INTRODUCTION

- Biodiesel production through transesterification is industrially done using acid or base homogeneous catalysts. Improvement could be achieved with other catalysts offering an environmental friendly process.
- ✓ This work describes the preparation of a novel catalyst to run the reaction at mild conditions.



TRANSESTERIFICATION REACTION



FAME = Fatty acid methyl esters.



FEEDSTOCK

First generation feed stocks such as corn oil, palm oil, rapeseed oil and soy bean oil, are commonly used for biodiesel because of their availability. But food and economic issues turn the biodiesel production unsustainable through time.





HOMOGENEOUS CATALYST

- \checkmark High yields.
- ✓ Fast reaction rates^[1].
- ✗ Difficulty on catalyst separation step.
- **×** Commonly as a two step reaction.

HETEROGENEOUS CATALYST

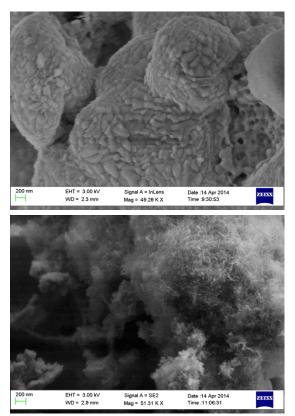
- ✓ One step reaction.
- \checkmark Simple catalyst separation step.
- \checkmark Possibility of regeneration and recycling.
- × Lower yields and harder reaction conditions.



CATALYST CARRIERS

Mayenite (Ca₁₂Al₁₄O₃₃) 2θ: 17-33° ^[2] Mesoporous ^[3]

Alumina (Al₂O₃) 2θ: 26-35-43-57° ^[2] Mesoporous ^[3]





CATALYTIC MATERIAL

Magnesium oxide (MgO) 2θ: 43-62°^[2] Largely used in solid catalysts for biodiesel production.

Lithium oxide (Li_2O) 20: 33-39-56-67°^[4] Less reported.



CATALYSTS SYNTHETIZED

The prepared catalysts (support-impregnating oxide):

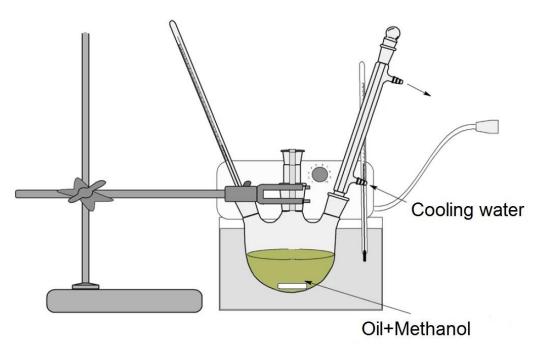
- 1. Alumina-MgO (5 30 wt.%)
- 2. Alumina-Li₂O (5 10 wt.%)
- 3. Mayenite-MgO (5 30 wt.%)
- 4. Mayenite- $Li_2O(5 10 \text{ wt.}\%)$

Stoichiometric quantities of the species are mixed with isopropanol, dried at 100 °C and calcinated at 650 °C for 2 h.



TRANSESTERIFICATION

The experimental set up:





TRANSESTERIFICATION

The conditions:

Methanol to oil ratio 6:1, heated up to 60 °C and stirred at 180 rpm for 2 h.

The variables:

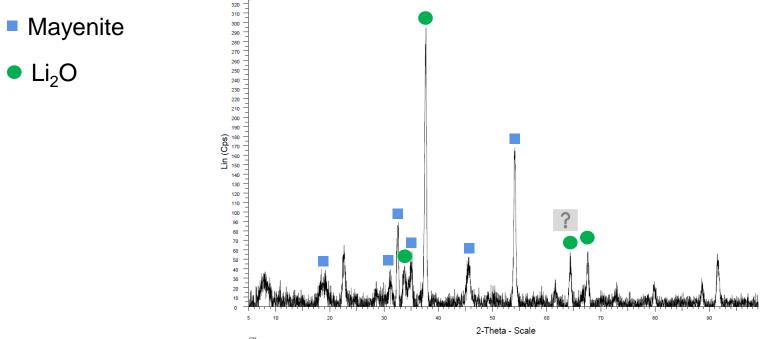
- > Oxide impregnation over catalyst (5 10 30 wt.%)
- Amount of used catalyst relative to oil (2.5 5.0 10.0 wt.%).
- Reusability for a second time for the catalyst with the best biodiesel production.



- ✓ Catalyst characterization: N₂ adsorption Brunauer– Emmett–Teller (BET), powder X-ray diffraction (XRD) and Scanning electron microscope (SEM).
- ✓ Catalyst performance: The product is analysed on Gas Chromatography.

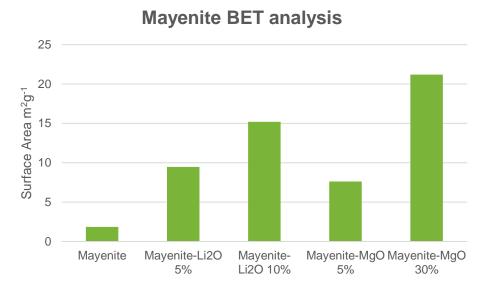


✓ XRD analysis, qualitatively confirms the presence of the expected species. The case of Mayenite-Li₂O 10%



Mayenite Li2O method 2 - File: Johanes20140516_A9_MayeniteLi2O_Meth2.RAW - Type: 2Th/Th locked - Start: 5.000 * - End: 100.000 * - Step: 0.020 * - Step time: 1. s - Temp: 25 *C (Room) - Time Started: 7 s - 2 Operations: Background 1.000,1.000 | Import





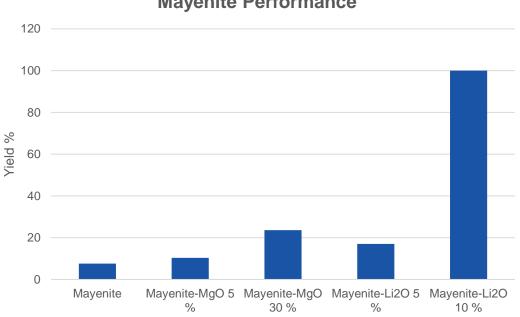
✓ Reported catalysts like Mg/MCM-41 that have 1289 m²g⁻¹ of surface area but achieve a maximum of 89 % biodiesel yield [5], also using low frequency ultrasonic waves and high rate stirrer.



- ✓ Mayenite alone and oxide impregnated show BET porosity from 11.9 to 40.1 Å placing them as mesoporous. The lowest is Mayenite-MgO 30% and the highest Mayenite-Li₂O 10%
- ✓ Alumina alone and oxide impregnated show BET porosity between 16.5 and 18.3 Å, suggesting that they are also mesoporous.



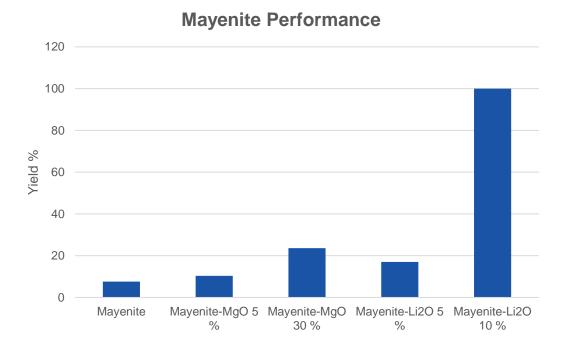
 \checkmark The best catalyst for biodiesel production is Li₂O 10% impregnated mayenite charged up to 5 wt.% relative to oil.



Mayenite Performance

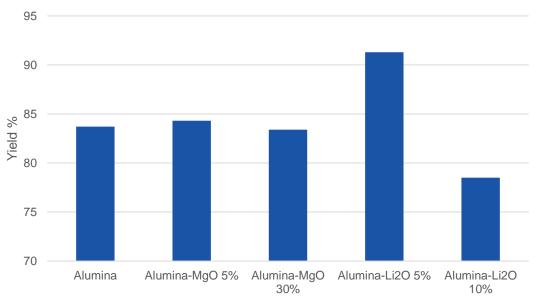


✓ The patent granted to Delfort et al., 2006 reports [6], achieve a yield of 94 % at 200 °C and 50 bar.





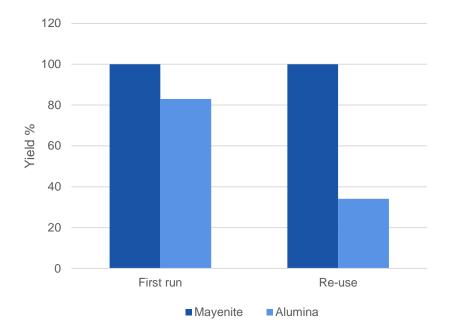
✓ Alumina alone used as a catalyst in the transesterification reaction has a relatively high biodiesel yield.



Alumina performance



✓ Re-usability tests have shown that Mayenite-Li₂O 10% can be used twice.



Re-usability performance



CONCLUSIONS

- ✓ Mayenite-Li₂O 10% catalyst has a yield of 100 % at 60 °C 180 rpm and at atmospheric pressure.
- Magnesium oxide impregnated over both studied carriers has a poor catalytic activity.
- ✓ Reusability is feasible for two times usage with Mayenite-Li₂O 10% catalyst, further studies must be carried to determine maximum reuse.



FURTHER STUDIES

- Transesterification nowadays is based in first generation feedstocks, such as soy bean oil, palm oil and canola oil^[7].
 For further studies, 2nd generation feedstock oils must be studied, e.g., from castor oil^[8].
- ✓ Maximum reuse and the best recovery method for Mayenite-Li2O 10% catalyst must be determined.



THANKS FOR YOUR ATTENTION!

ANY QUESTIONS?





REFERENCES

[1] Schuchardt, U., Sercheli, R., Vargas, M., 1998, Transesterification of vegetable oils: a review: Journal of Brazilian Chemistry Society, v. 9, p. 199-210

[2] http://www.mineralienatlas.de/. Visited on August, 2014

[3] Kaneko, K., 1994, DETERMINATION OF PORE- SIZE AND PORE- SIZE DISTRIBUTION . 1. ADSORBENTS AND CATALYSTS, J. Membr. Sci., p. 59-89.

[4] Kessinger, G. F., Jurgensen, A. R., Missimer, D. M., Morrell, J. S., 2009, The High Temperature Chemical Reactivity of Li2O

[5] Georgogianni, K. G., A. P. Katsoulidis, P. J. Pomonis, and M. G. Kontominas, 2009, Transesterification of soybean frying oil to biodiesel using heterogeneous catalysts: Fuel Processing Technology, v. 90, p. 671-676.

[6] B. Delfort, D. Le Pennec, C. Lendresse, Process for transesterification of vegetable oils or animal oils by means of heterogeneous catalysts based on zinc or bismuth, titanium and aluminum. United State patent 7,151,187 B2 (2006).

[7] Jahirul, M. I., R. J. Brown, W. Senadeera, I. M. Hara, and Z. D. Ristovski, 2013, The use of artificial neural networks for identifying sustainable biodiesel feedstocks: Energies, v. 6, p. 3764-3806.

[8] Jahirul, M. I., R. J. Brown, W. Senadeera, I. M. Hara, and Z. D. Ristovski, 2013, The use of artificial neural networks for identifying sustainable biodiesel feedstocks: Energies, v. 6, p. 3764-3806.



Base Catalyst Mechanism Acid Catalyst Mechanism 1a R—ОН R3. RO⁻ H 1 1b R₂ R_2 R₁ R₂ R₂ 2 R₃ R R OF но R_2 °0⁺ RO H R_2 3 R₃. 'R R_3 R_3 3 R₃ R_2 R₁ НÒ °0

 R_1

+

-0

 R_2

0=

-M+ -M+-