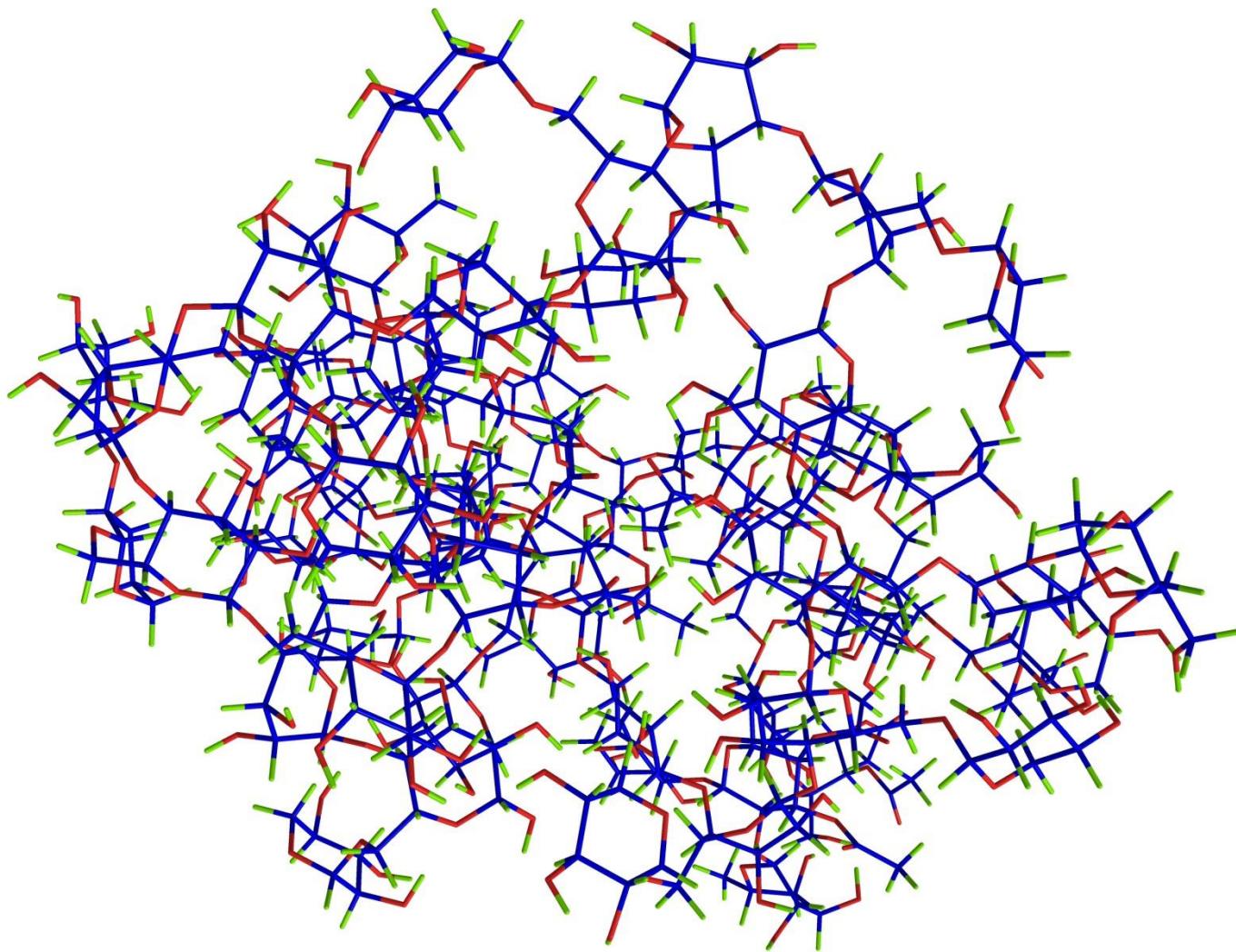
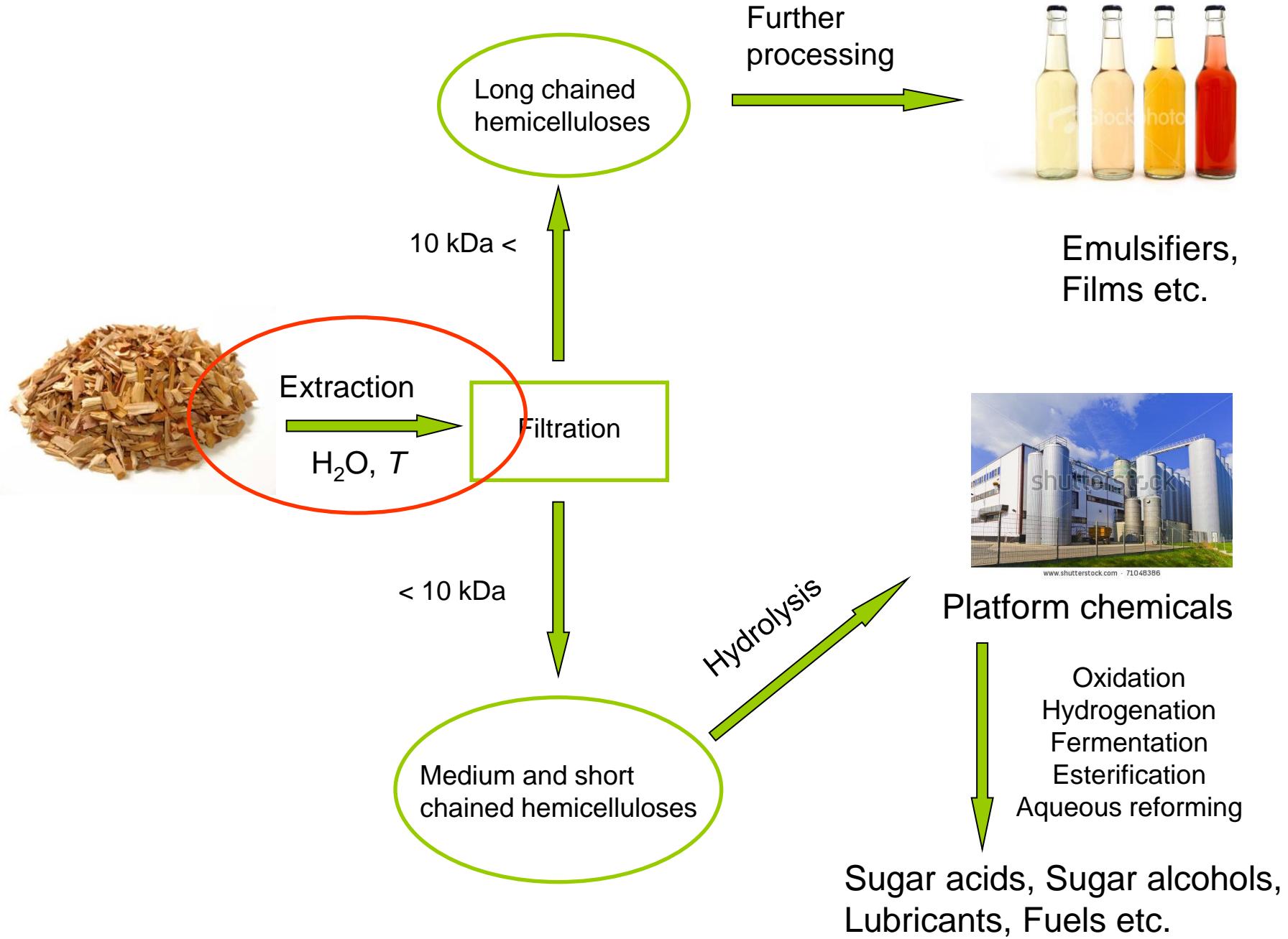


Extraction of spruce hemicelluloses

*J. V. Rissanen,
H. Grénman, D. Yu. Murzin, T. Salmi*

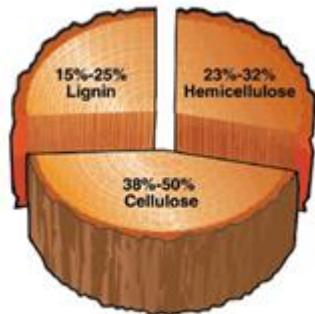
Hemicellulose molecule



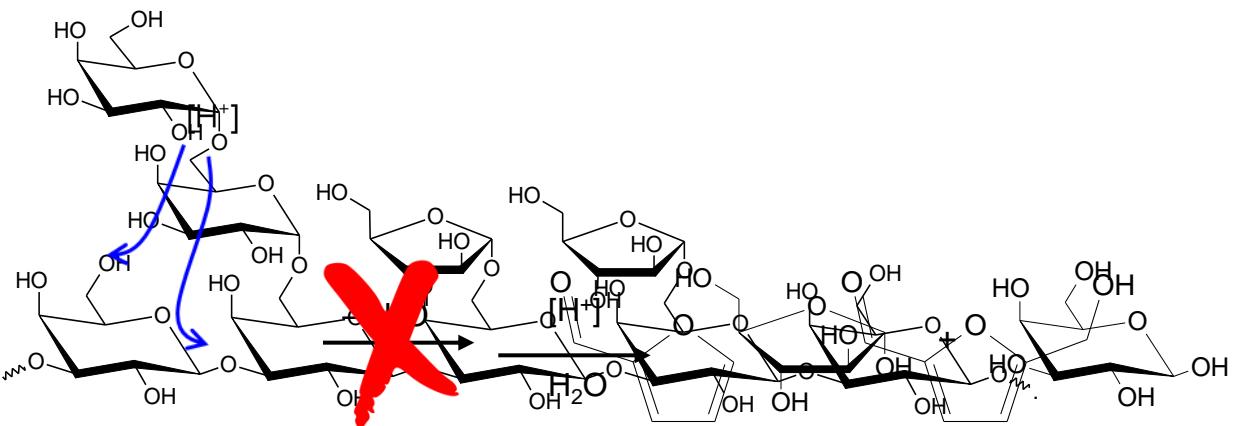


Background

- Protonation of glycosidic bonds



Wood



Starting material

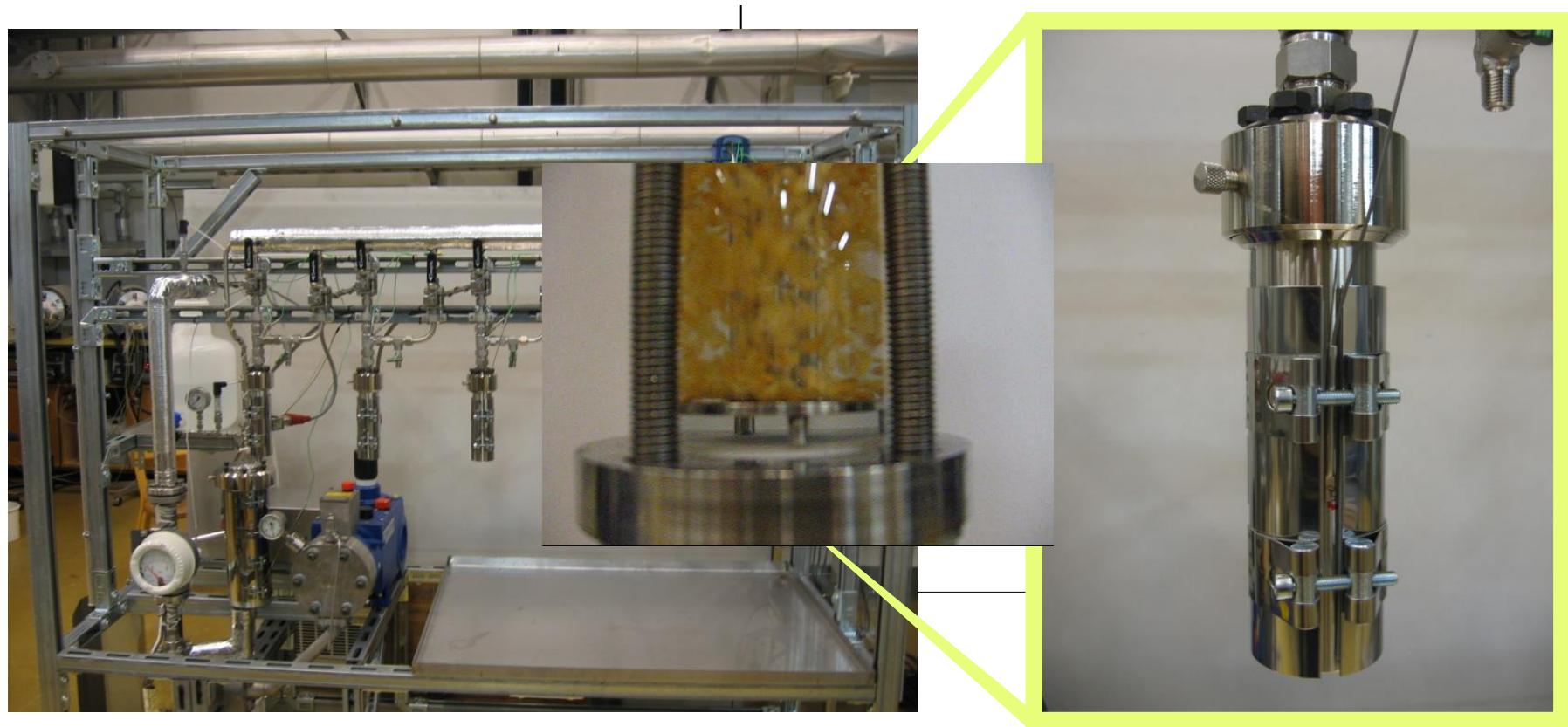


Non-extracted chips, 1.25 – 2 mm



Non-extracted cubic blocks, 10 mm

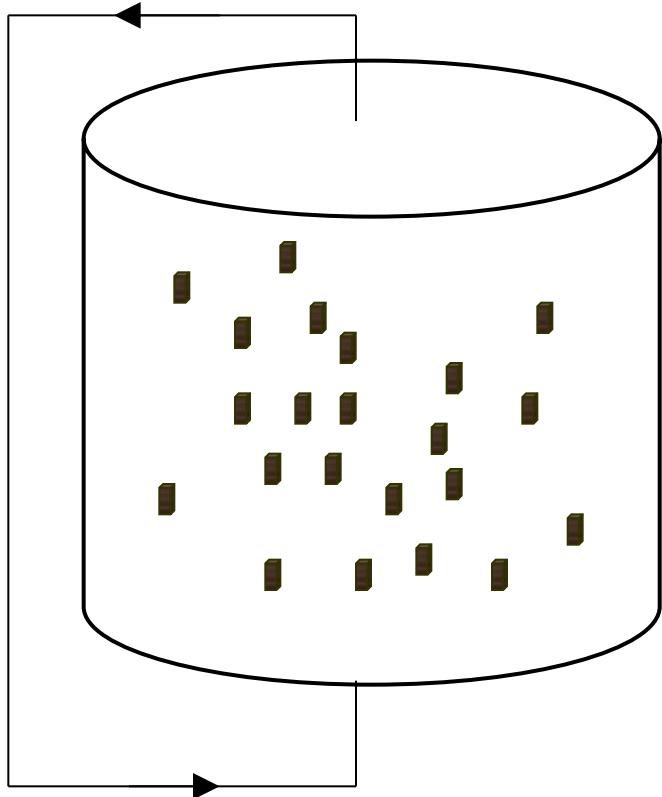
Reactor system



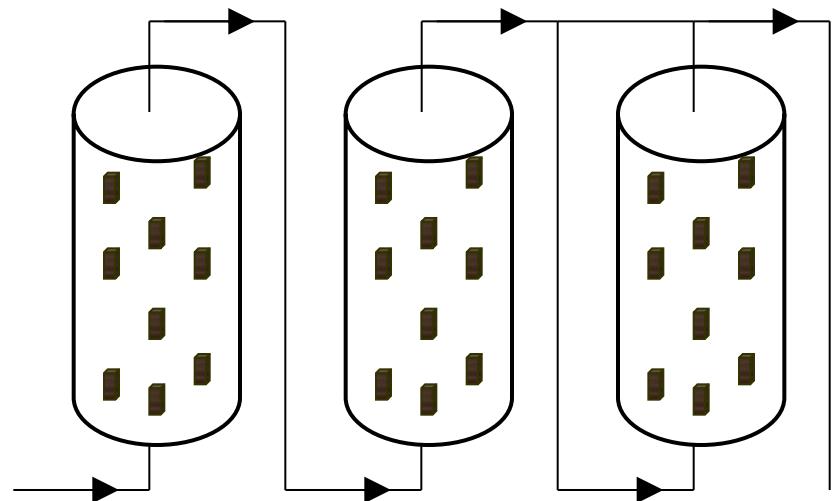
- Cascade reactor
- Flexible 5 point sampling of liquid and solid phases
- Accurate control and measurement of temperature, pressure and flow rate

Batch reactor versus cascade reactor

Traditional batch digester



Cascade reactor



The chips do not differentiate between reactor type

Liquid samples, 170°C, 0-60 min

5 min

10 min

15 min

20 min

60 min



- The viscosity of the extract increasing
- The color becomes brown

Solid samples, 170°C, 0-60 min

0 min



5 min



10 min



15 min



20 min

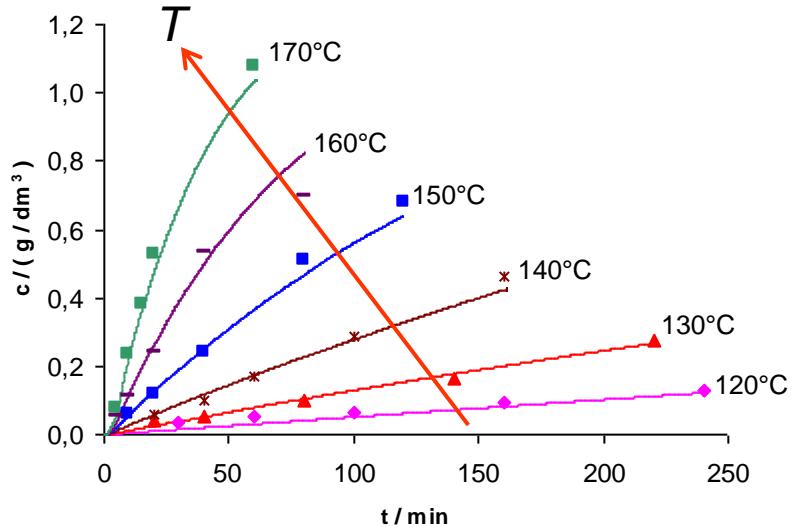


60 min

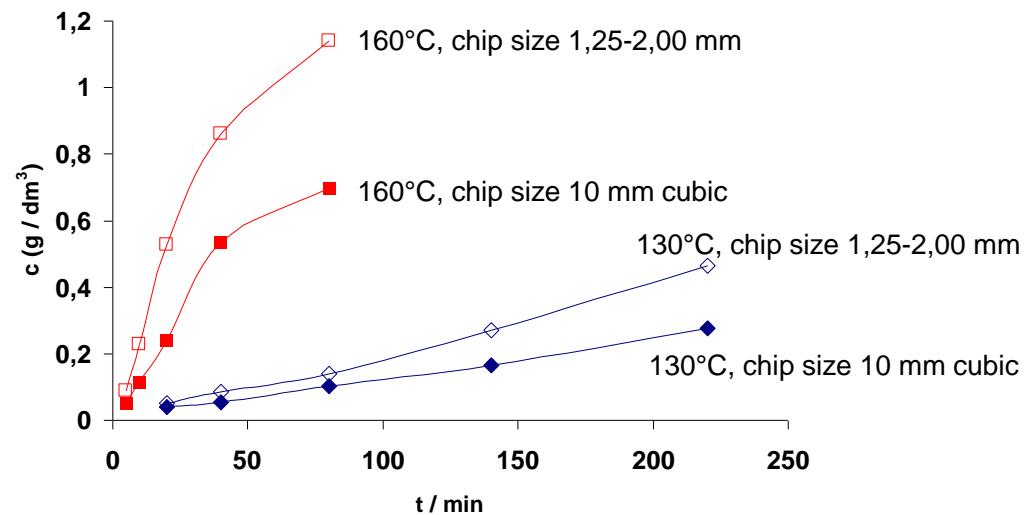


Experimental results

The influence of temperature and chip size on the overall extraction rate

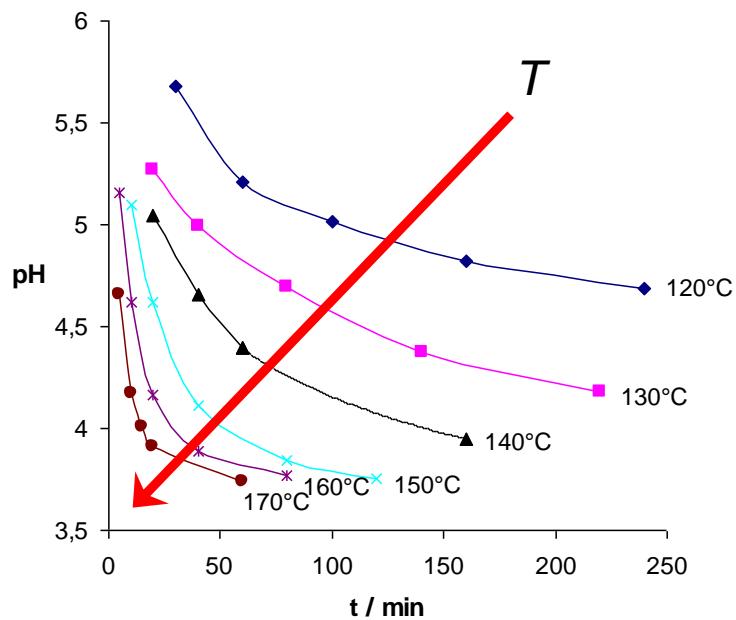


Concentration of hemicellulose as a function of time (10 mm cubic blocks).

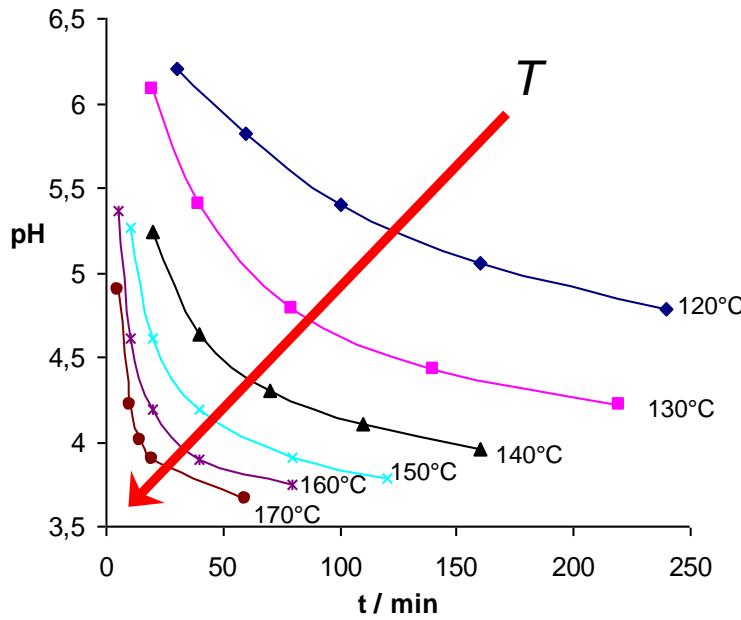


Liquid phase concentration as a function of time with different chip sizes.

The behaviour of pH during extraction



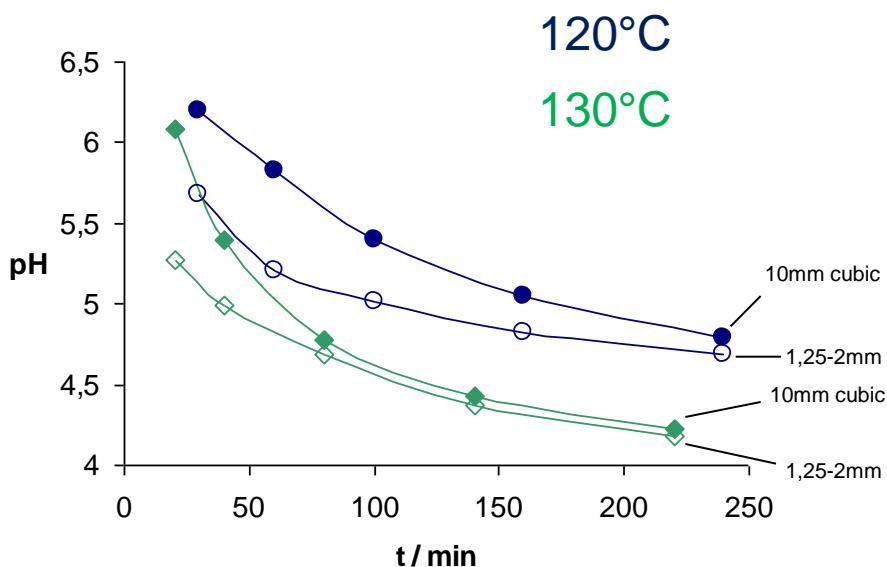
1,25 – 2,00 mm wood chips



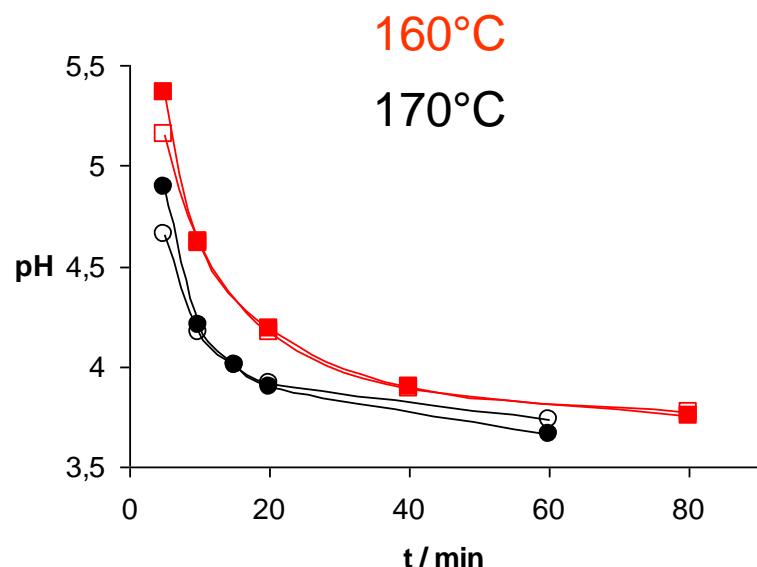
10 mm cubic wood blocks

Influence of chip size on pH

The behavior of the pH during the reaction at four different temperatures

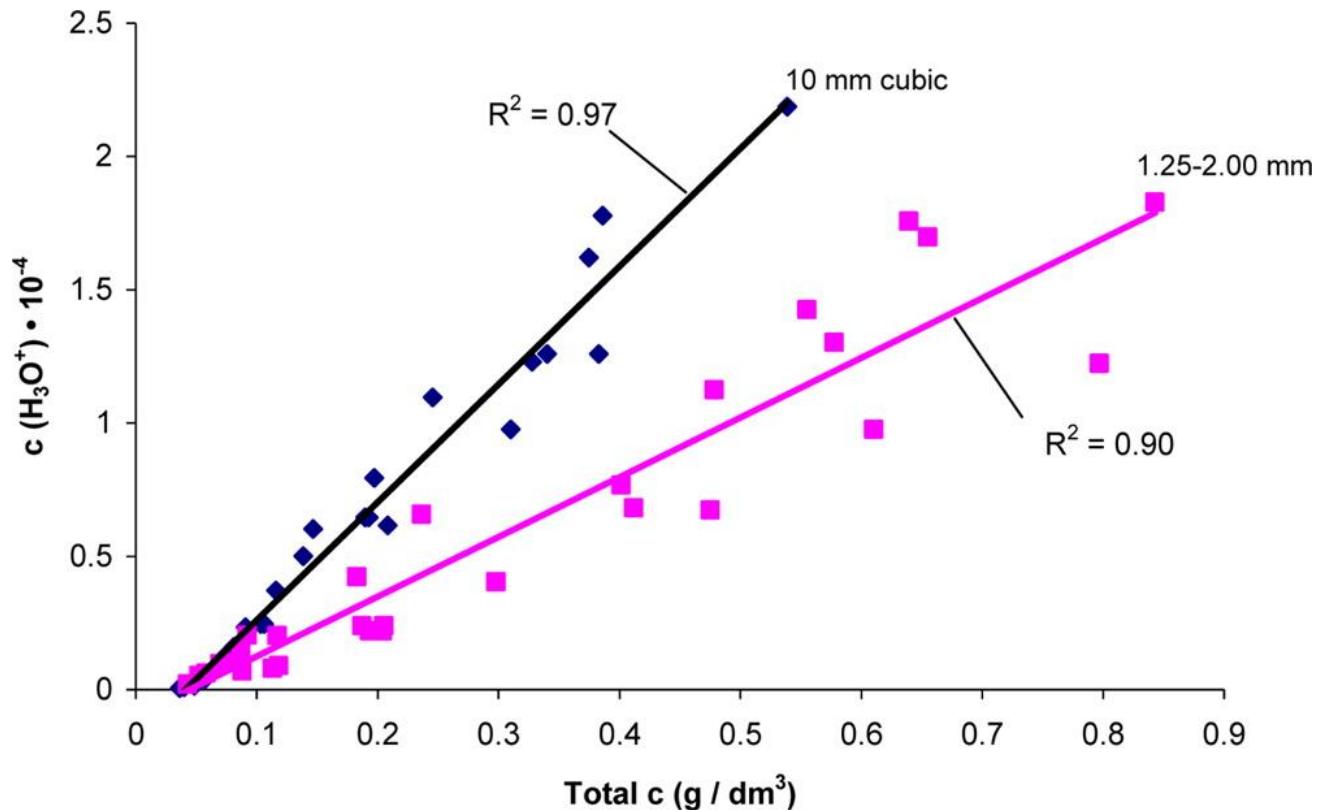


The pH with 1,25 – 2 mm chips (open symbols) and 10 mm cubic blocks (solid symbols).



The pH with 1,25 – 2 mm chips (open symbols) and 10 mm cubic blocks (solid symbols).

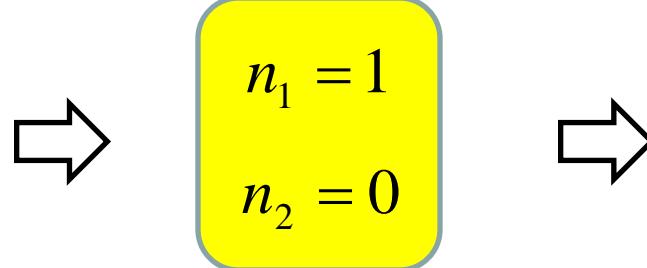
H_3O^+ vs total hemicellulosic sugars



- The diffusion of the acetyl groups is clearly faster than for the hemicelluloses i.e. higher CH_3O^+ is obtained at the same conversion for the larger chips

Modelling

$$rate = k_I \cdot c_{solid}^{n_1} \cdot (H^+)^{n_2}$$



$$k_I = k_{\theta I} \cdot e^{\frac{-E_{aI}}{RT}}$$

$$T = \frac{1}{T} - \frac{1}{T_{mean}}$$

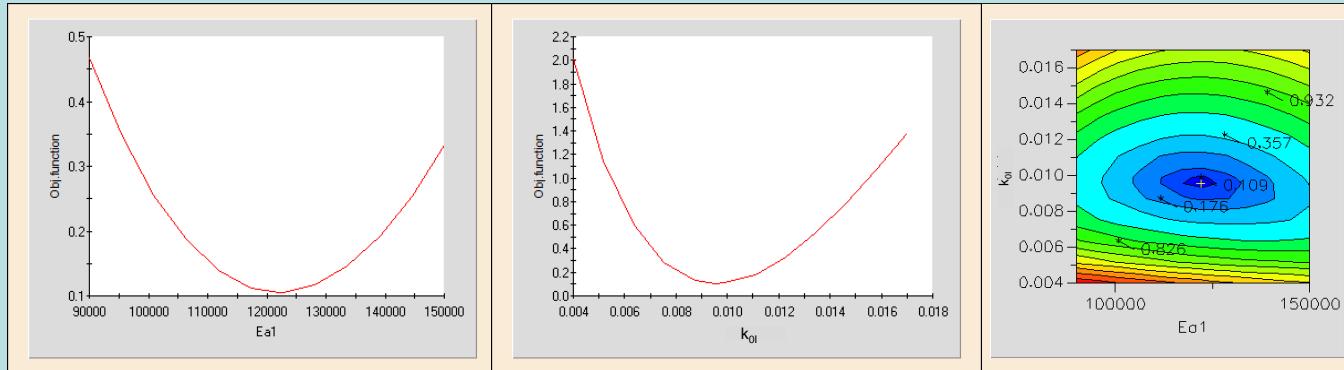
$$T_{mean} = 150^\circ C$$

	1,25 - 2,00 mm chips		10 mm cubic blocks	
	Estimated parameters	Estimated Std Error (%)	Estimated parameters	Estimated Std Error (%)
$E_a [\text{kJ / mol}]$	122	0,3	120	0,2
$k_{0I} [(L^{(n_1+n_2)-1}) / (g^{(n_1+n_2)-1} \cdot \text{min})]$	$9,57 \cdot 10^{-3}$	0,3	$5,55 \cdot 10^{-3}$	0,3

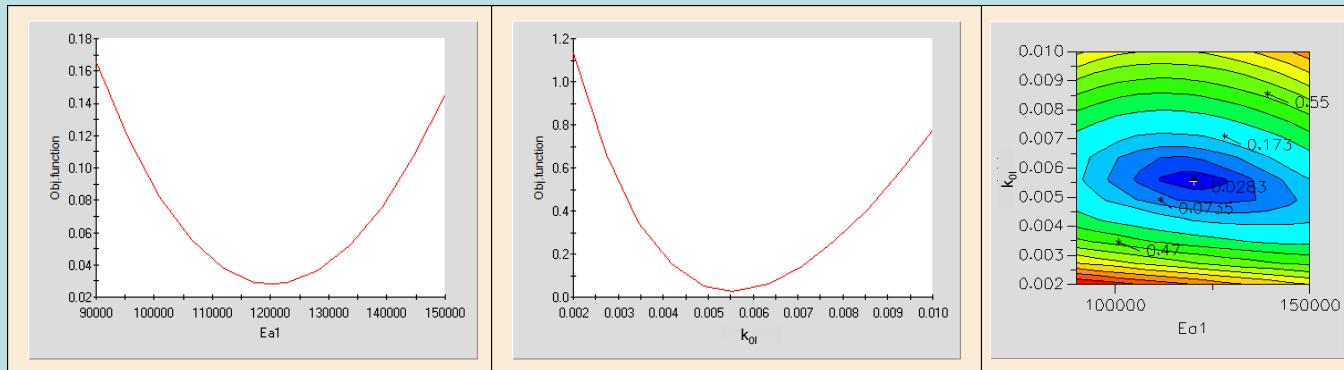
The model of the complicated system can be simplified significantly

Sensitivity analysis and parameter correlations (E_a and k_{O1})

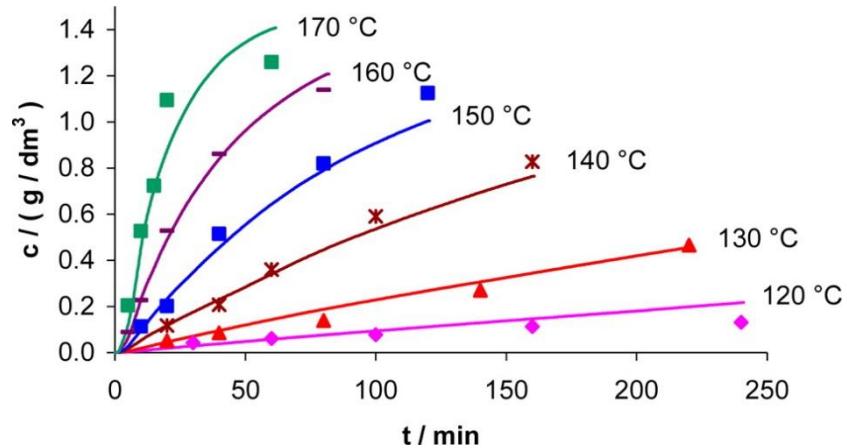
1,25 – 2,00 mm chips



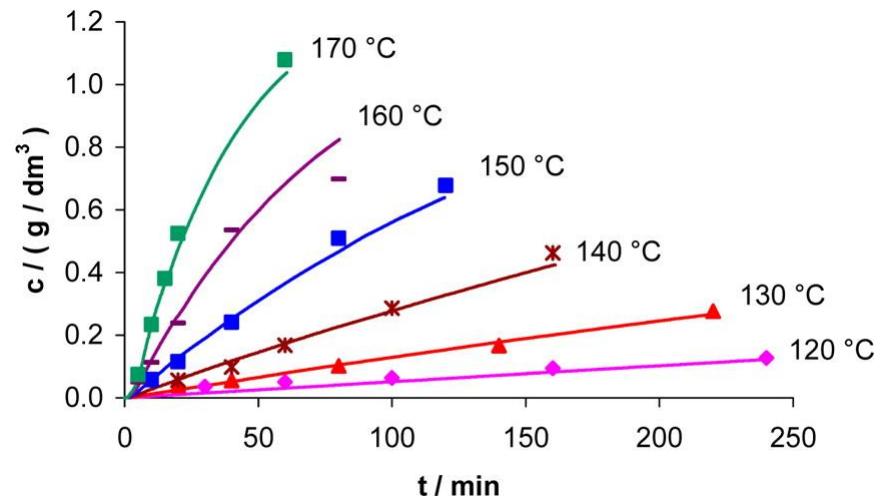
10 mm cubic blocks



Modelling results



Fit of the model to experimental data (liquid-phase hemicellulose concentrations c) for the smaller chip size (1.25–2 mm).



Fit of the model to experimental data (liquid-phase hemicellulose concentrations c) for the larger chip size (10 × 10 mm).

So what did we learn from modelling exercise?

- Extraction and hydrolysis rate very temperature sensitive
- The chip size influences the overall extraction rate and the molar mass of the obtained hemicelluloses
- The extraction rate is not significantly influenced by pH
- The mathematical model for the complex system could be simplified significantly
- A good fit of the model to the experimental data was achieved

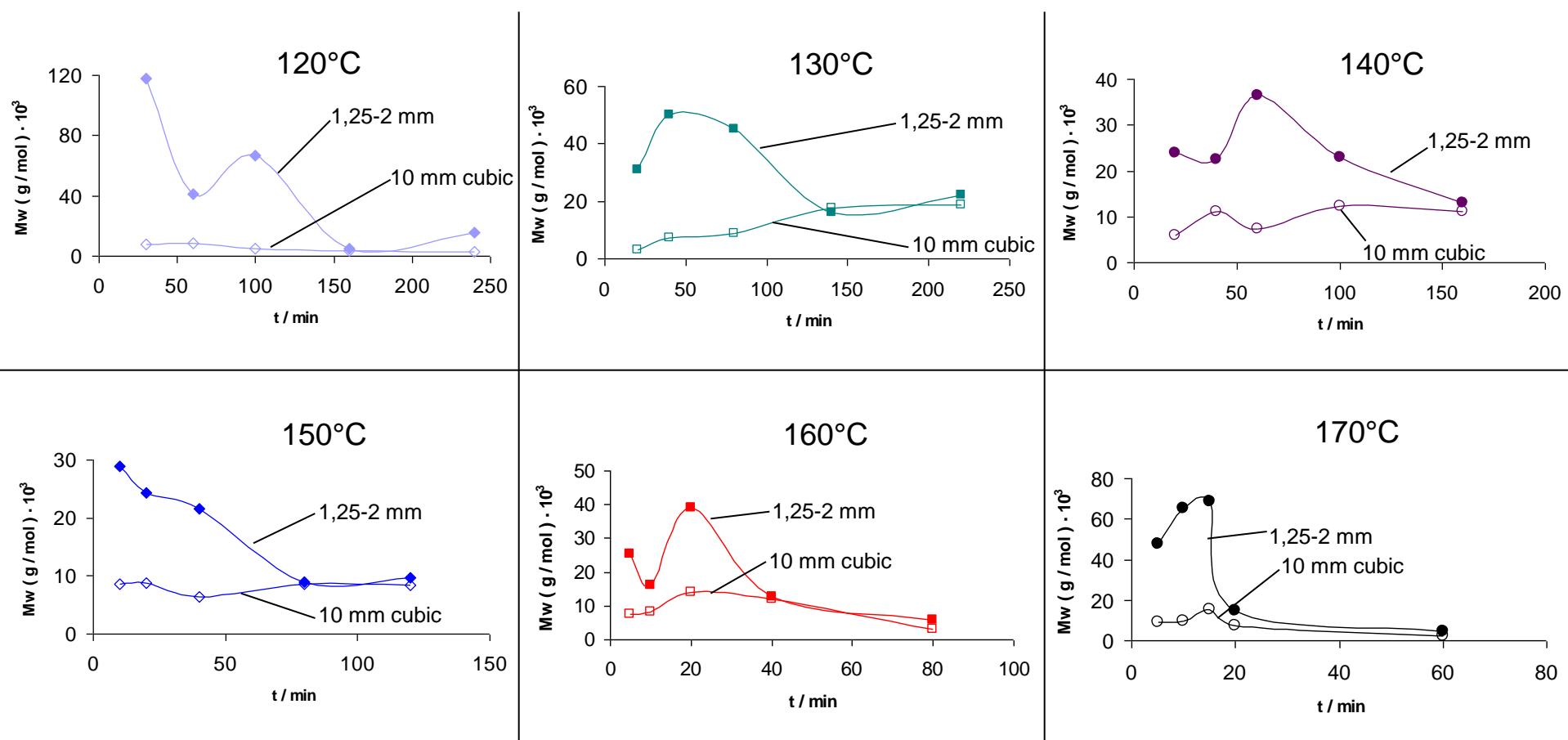
Rissanen, Grénman, Willfor, Murzin, Salmi, Industrial & Engineering Chemistry Research (2014), 53(15), 6341-6350.

Rissanen, Grénman, Xu, Willför, Murzin, Salmi, ChemSusChem 2014, accepted, DOI 10.1002/cssc.201402282R1

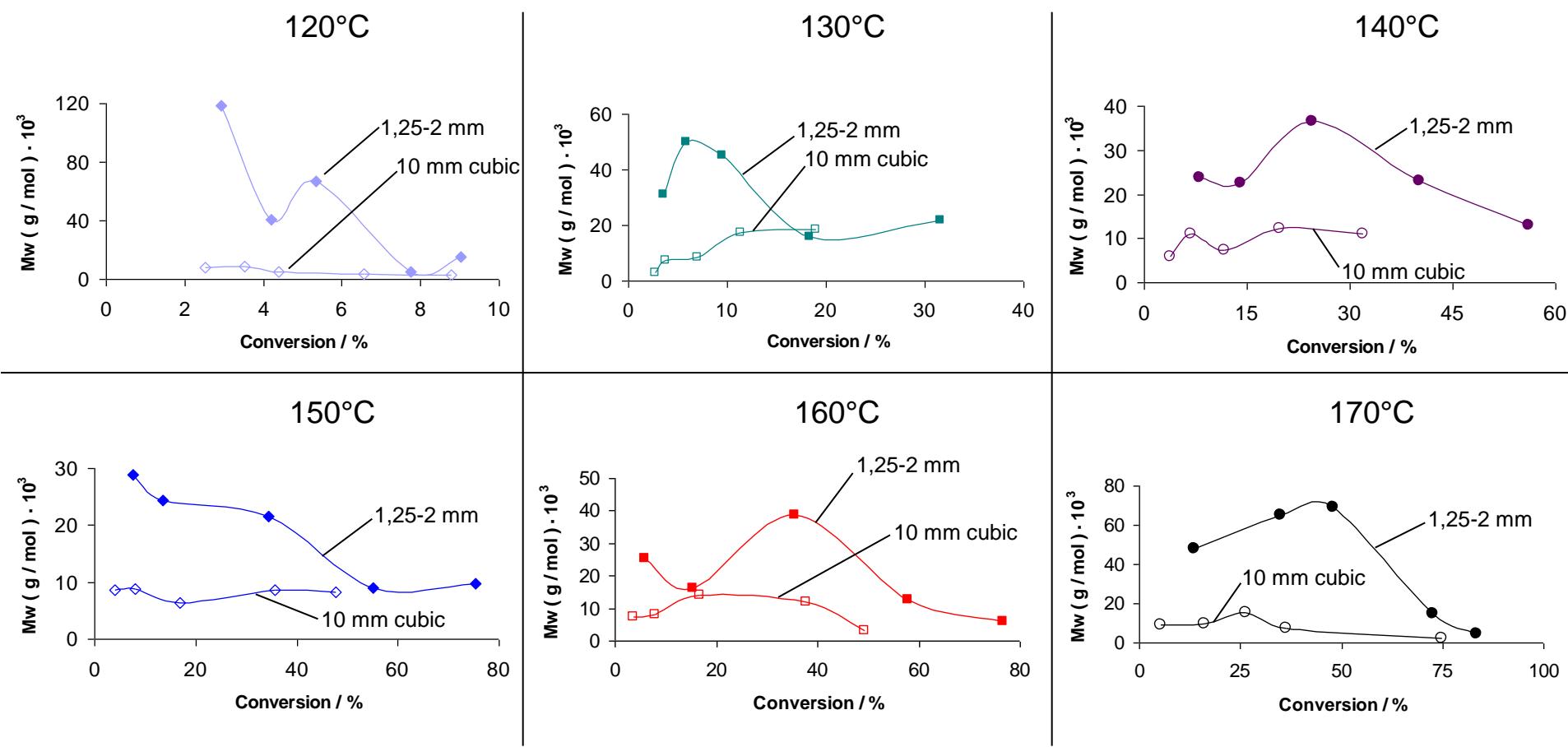
Rissanen, Grénman, Xu, Willför, Murzin, Salmi, Cellulose Chemistry and Technology, submitted after revision

Molar mass of extracted hemicelluloses

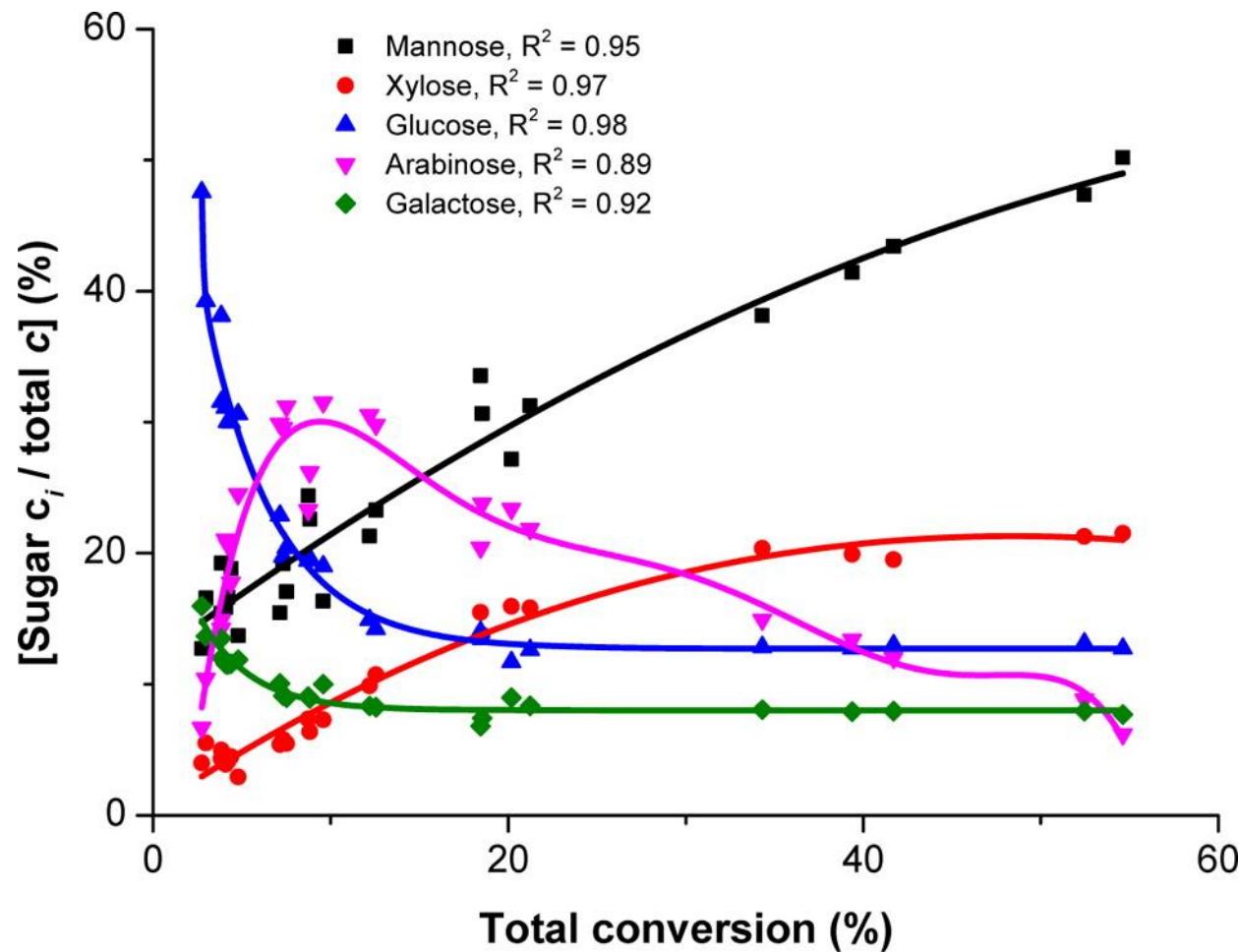
Molecular weight as a function of time for different temperatures and chip sizes



Molecular weight as a function of conversion for different temperatures and chip sizes



Percentage of sugars in the extract, 120–170° C



Conclusions

- Industrial applications need long chained hemicelluloses and monomers
- The extraction kinetics is crucial in order to tailor the product as well as the production
- The overall extraction is influenced by several interlinked phenomena

Rissanen, Grénman, Willfor, Murzin, Salmi, Industrial & Engineering Chemistry Research (2014), 53(15), 6341-6350.

Rissanen, Grénman, Xu, Willför, Murzin, Salmi, ChemSusChem 2014, accepted, DOI 10.1002/cssc.201402282R1

Rissanen, Grénman, Xu, Willför, Murzin, Salmi, Cellulose Chemistry and Technology, submitted after revision

Conclusion –

The influence of the extraction parameters is complex and interlinked

