

COST FP0901

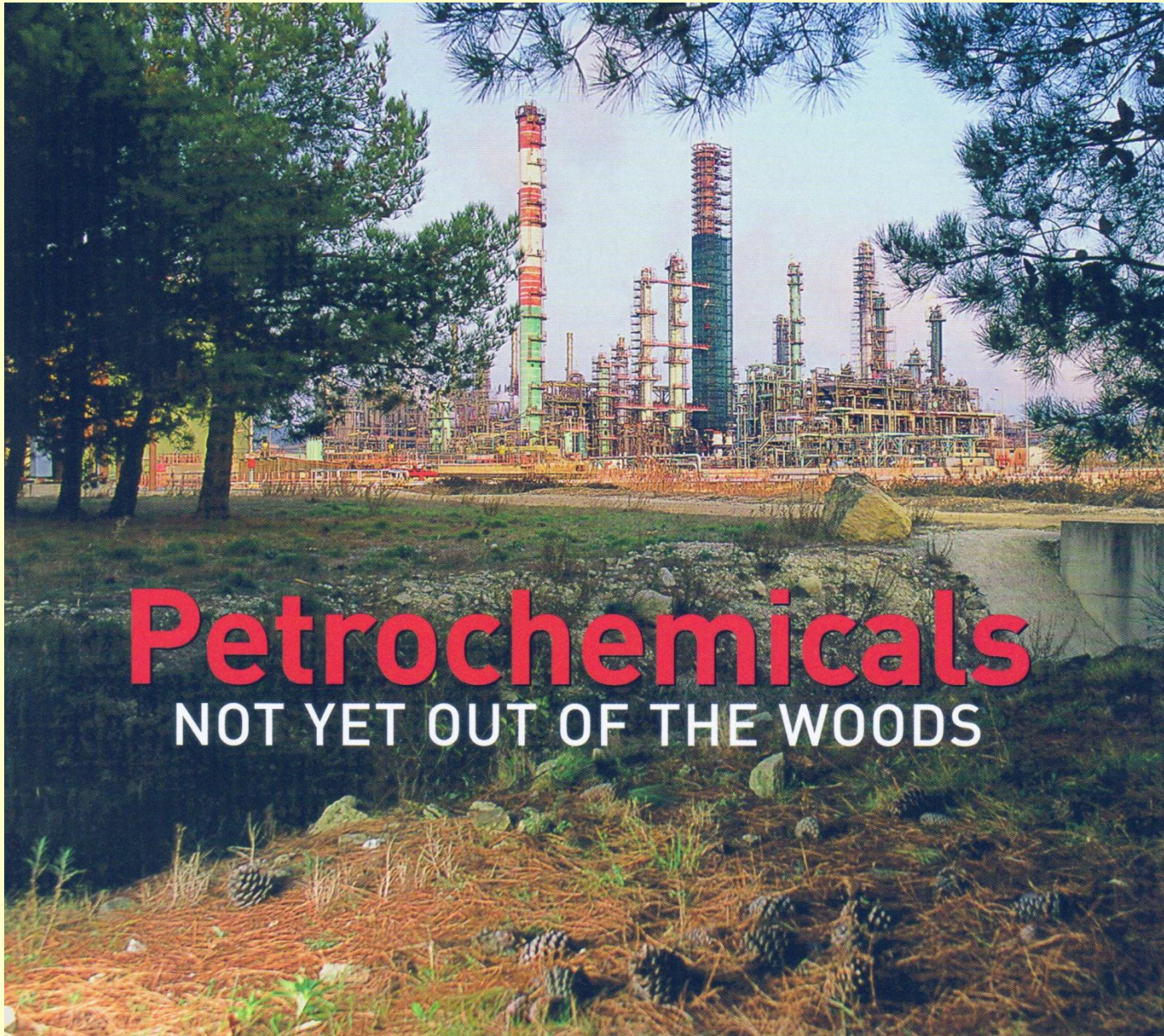
Non-sulphur lignin studies under general biorefinery concept and evaluation of energy consumption by steam explosion

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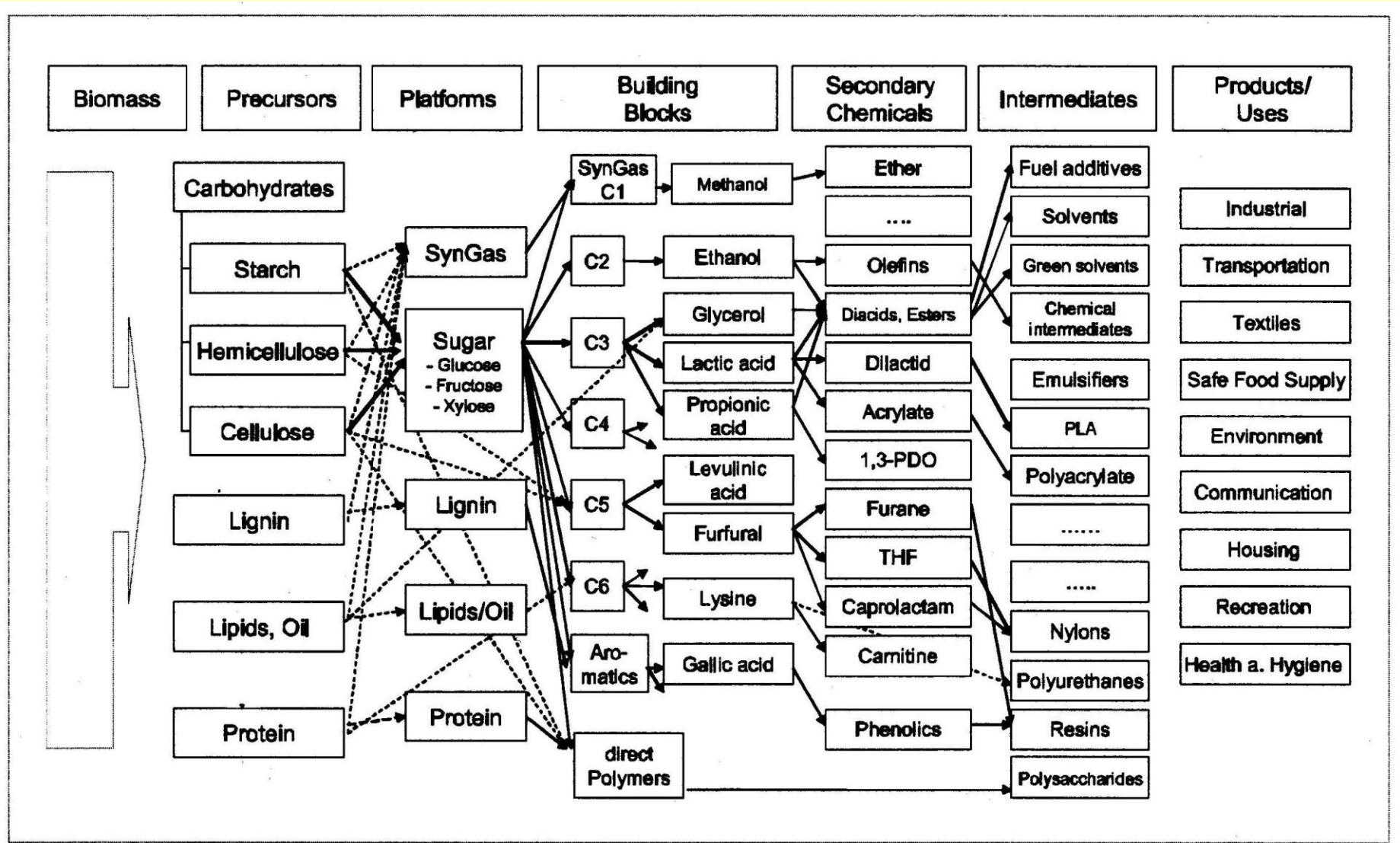


Petrochemicals

NOT YET OUT OF THE WOODS

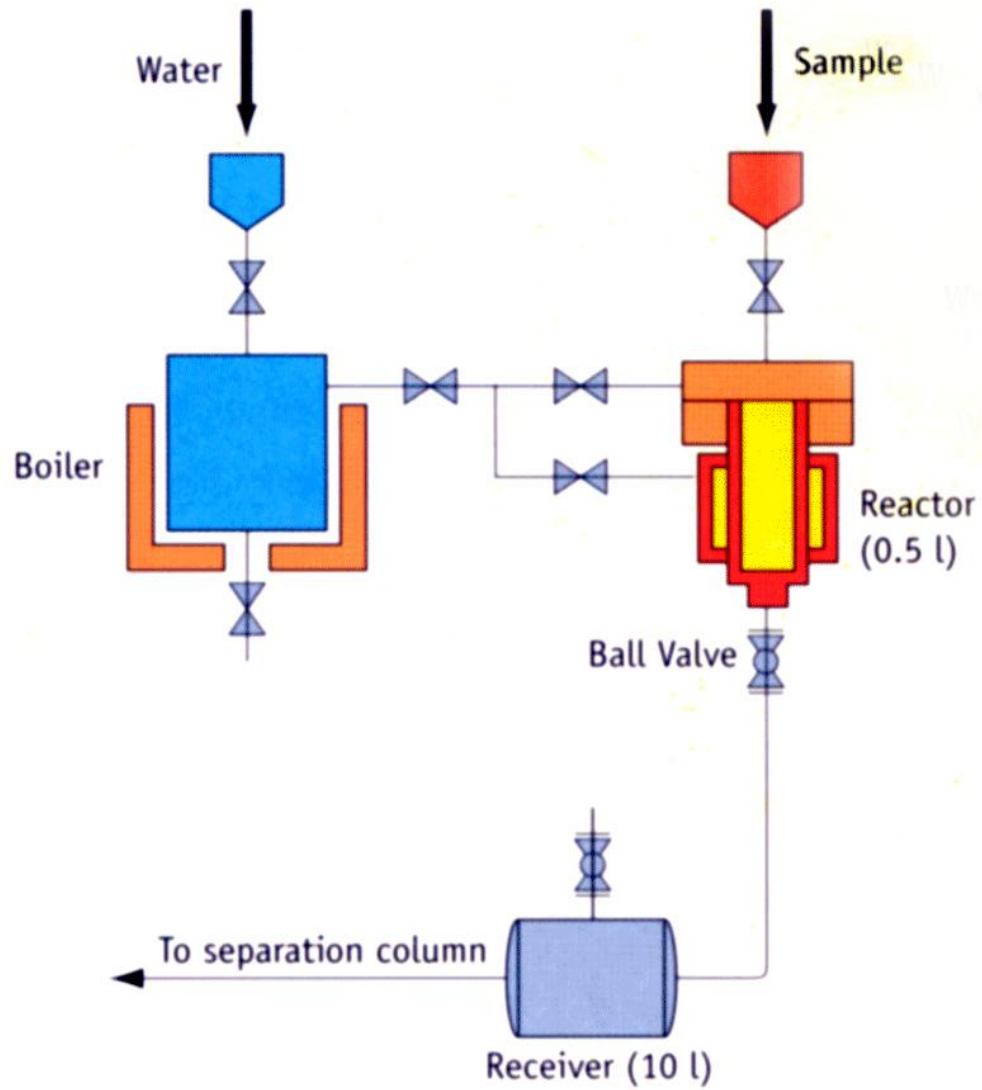
What is biorefinery?

- **A biorefinery is a technologies cluster, which integrates biomass conversion into transportation fuels, power, chemicals and advanced materials within zero emissions framework. (LSIWC/LBE-EC)**
- **„Biorefineries combine the necessary technologies between biological raw materials and industrial intermediates and final products. The principal goal in the development of biorefineries is defined by the following: (biomass) feedstock-mix + process-mix → product-mix” (Kamm)**



Adapted from Kamm

Steam Explosion Unit



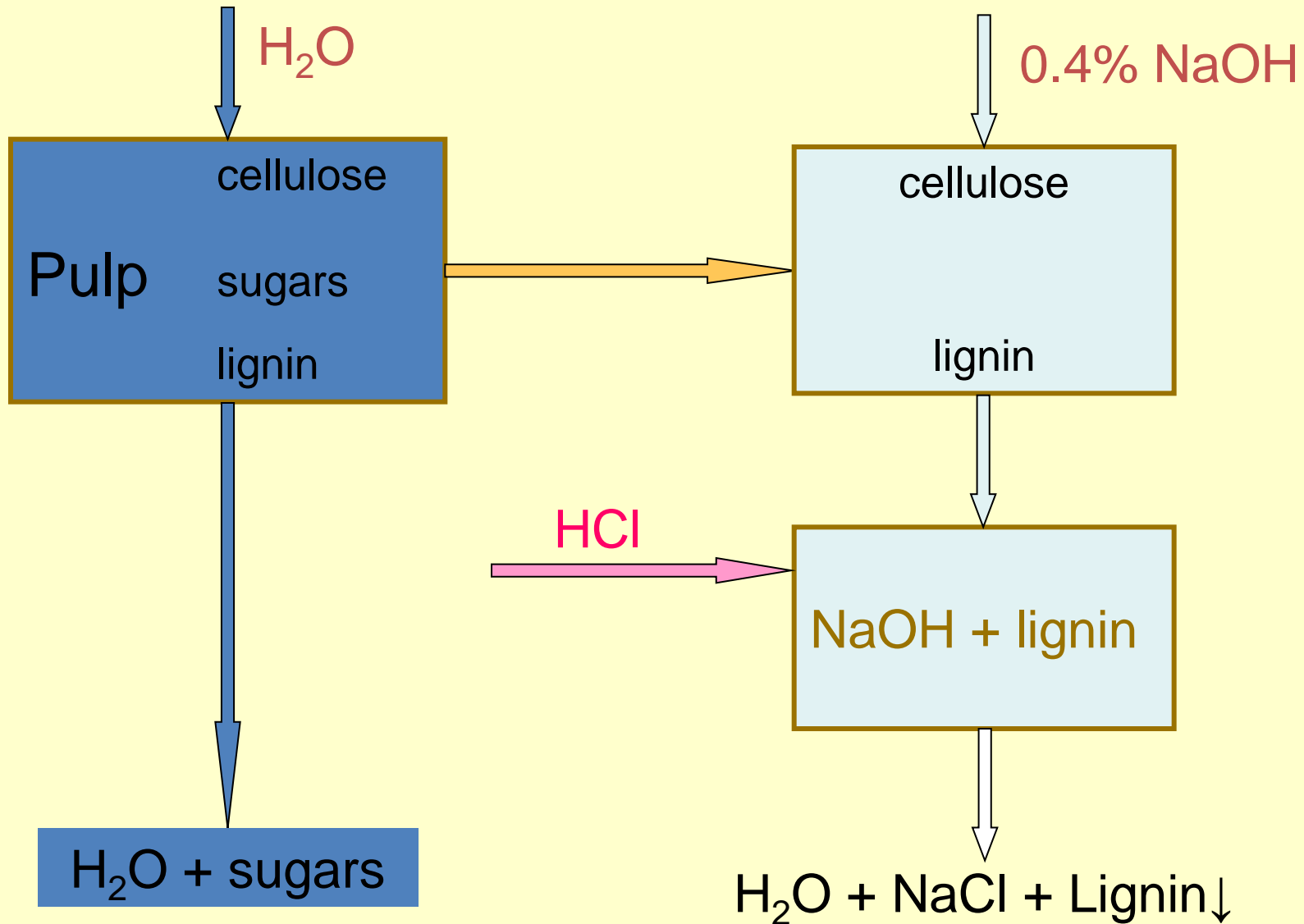
Steam Generator



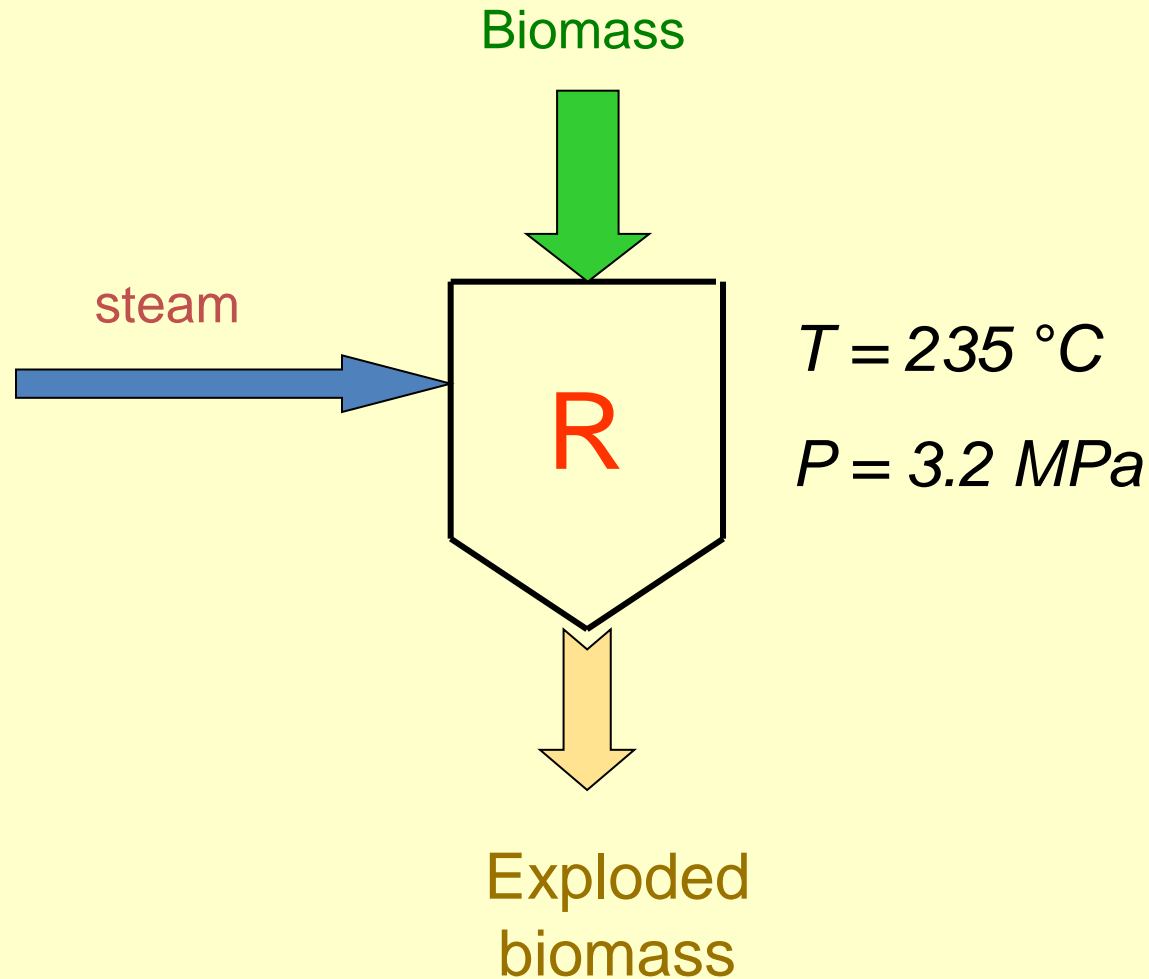
Reactor



Extraction of lignin



Steam explosion auto-hydrolysis



Non-sulphur lignins

Grey Alder, SE lignin:

SE treatment conditions: N1 – 1 min; N2 – 2 min, N3 – 3 min

Birch lignin:

N4 – SE

N5 Bjorkman's lignin

N6 *Wheat straw SE lignin*

PY-GS/MS

At-1701, 60m	Grey Alder, SE lignin			Birch lignin		Wheat straw lignin
MS_mod_PY sp15 . PY 500°C(1,04-1,10mg)	Different SE conditions			SE	Bjorkman's	SE
MS dati (Integration: 300/30000)						
06-07/ 07-2010	N1	N2	N3	N4	N5	N6
Carbohydrates(C)	1,92	2,07	2,29	1,33	5,67	2,27
Lignin (L)	51,42	46,86	43,57	51,29	54,39	39,92
Summa C+L=100%	53,34	48,93	45,86	52,62	60,06	42,19
Carbohydrates, % from C+L	3,6	4,23	4,99	2,53	9,44	5,38
Lignin, % from C+L	96,4	95,77	95,01	97,47	90,56	94,62
C/L	0,037	0,044	0,053	0,026	0,104	0,057

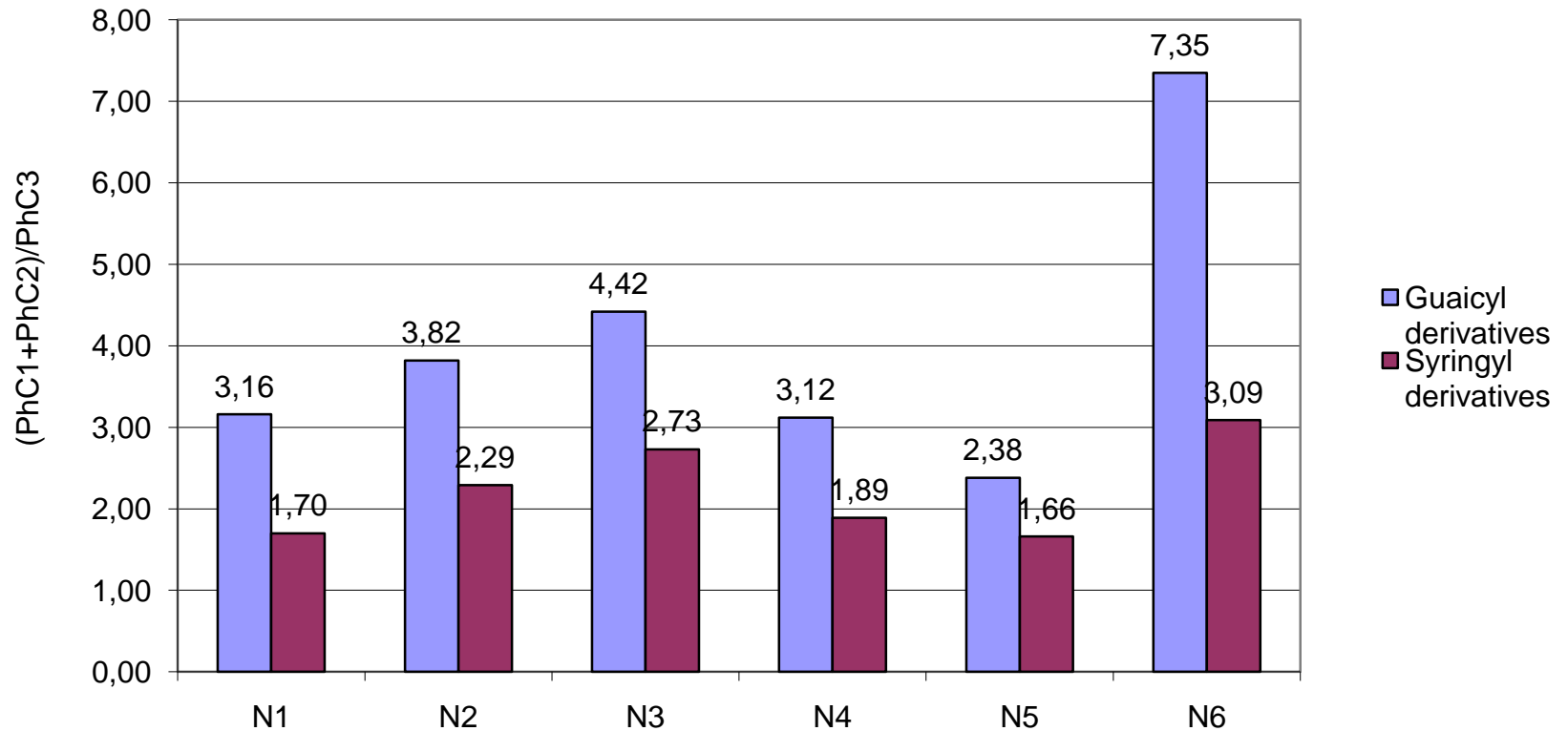
PY-GS/MS

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MS dati (Integration: 300/30000)						
06-07/ 07-2010	N1	N2	N3	N4	N5	N6
Carbohydrates (C), 100%	% from total C					
Acid, Ester, Ether	31,25	40,1	39,3	46,62	59,79	39,21
Aldehyde, Ketone	38,54	32,37	25,33	33,08	24,69	35,24
Alcohol					2,12	
Furan	19,27	22,22	34,06	15,04	10,05	20,7
Pyran	10,94	5,31	1,31	5,26	3,35	4,85

PY-GC/MS

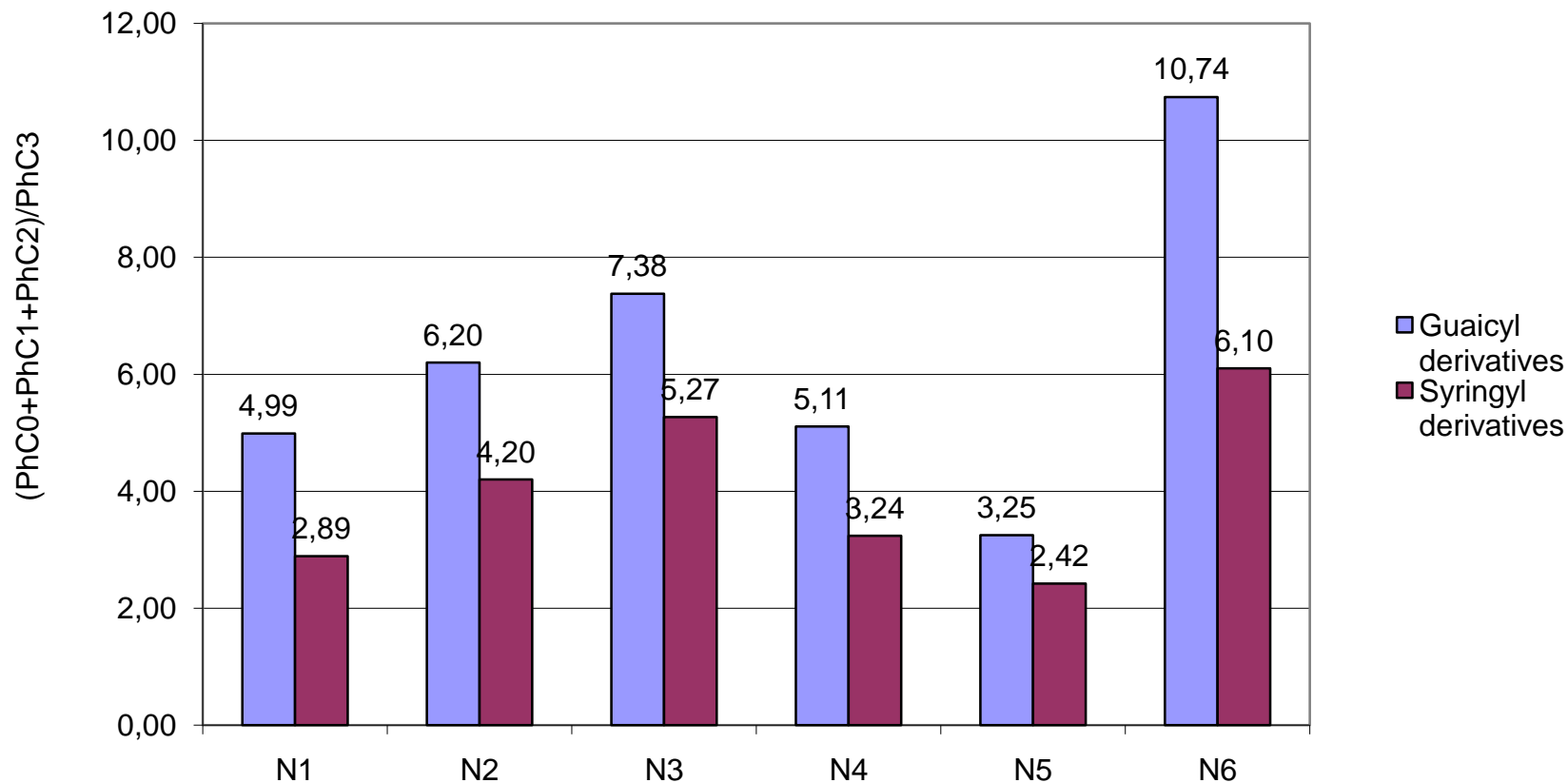
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MS_mod_PY sp15 . PY 500°C(1,04-1,10mg)	Different SE conditions			SE	Bjorkman's	SE
MS dati (Integration: 300/30000)						
06-07/ 07-2010	N1	N2	N3	N4	N5	N6
Lignin(L), 100%	% from total L					
Phenyl and benzyl derivates,	5,74	6,34	6,72	2,87	2,61	10,28
Guaiacyl -	25,71	28,96	29,57	19,71	24,31	59,89
Syringyl -	68,55	64,7	63,71	77,42	73,08	29,83

Phenylmethane(PhC1)+phenylethane(PhC2)/phenylpropane(PhC3) ratio
for S-type phenols calculated on the basis of Py-GC/MS of samples



PY-GS/MS

Phenyl(PhC0)+phenylmethane(PhC1)+phenylethane(PhC2)/phenylpropane (PhC3) ratio for S-type phenols calculated on the basis of Py-GC/MS of samples



SE self-binding MDF hot pressing

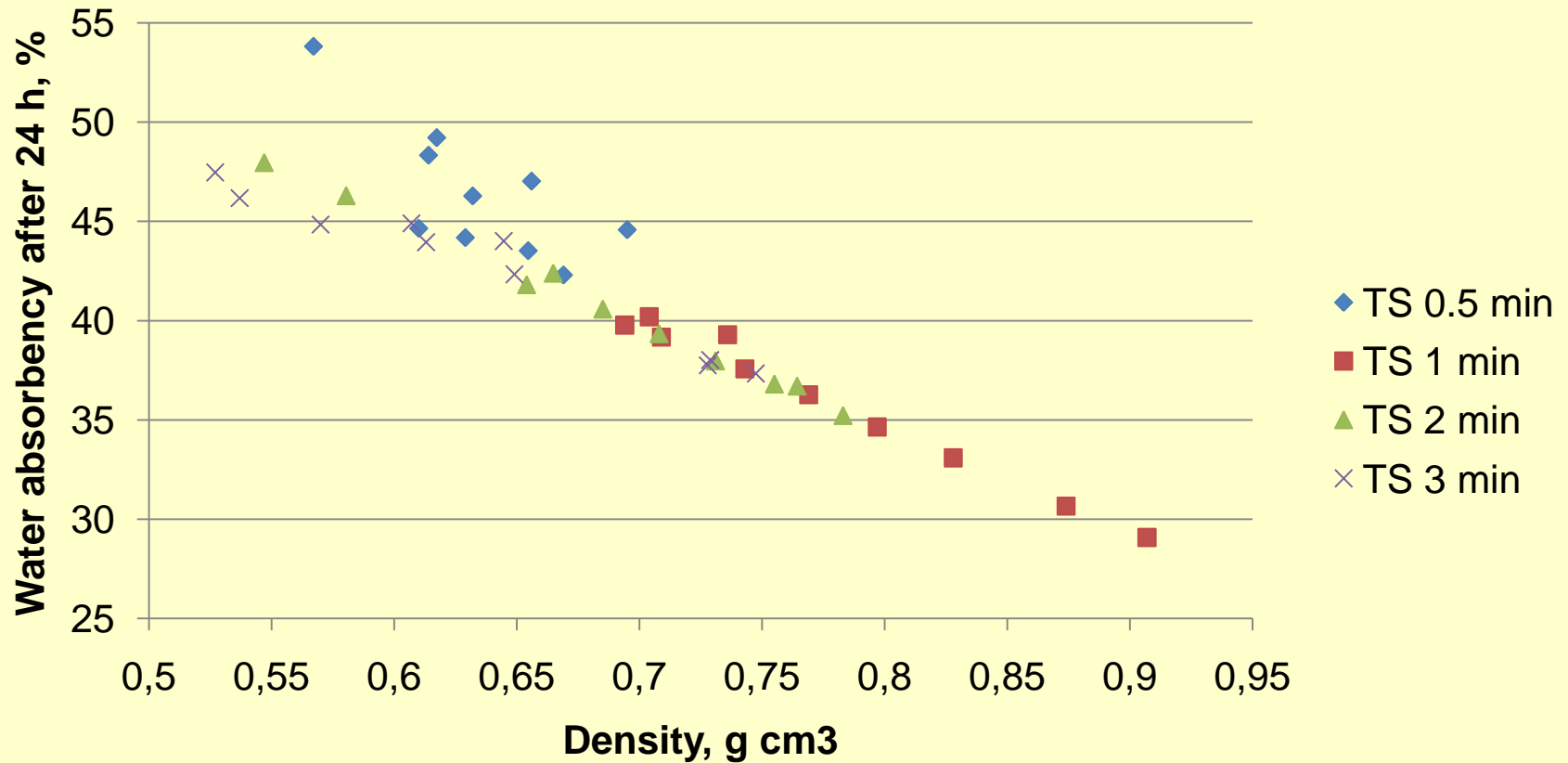


Sample	T, °C	p, Mpa max/min	Time, min (hot+cool)
SE 05	160	0.6/0.05	8 + 10
SE 1	150	0.8/0.08	8 + 15
SE 1	160	1.5/0.02	8 + 12
SE 1	170	2.1/0.02	6 + 10
SE 2	160	0.6/0.05	8 + 10
SE 3	160	0.4/0.06	8 + 10



Form Stability vs Density

SE MDF (160 °C)



Consumption of energy

Net efficiency

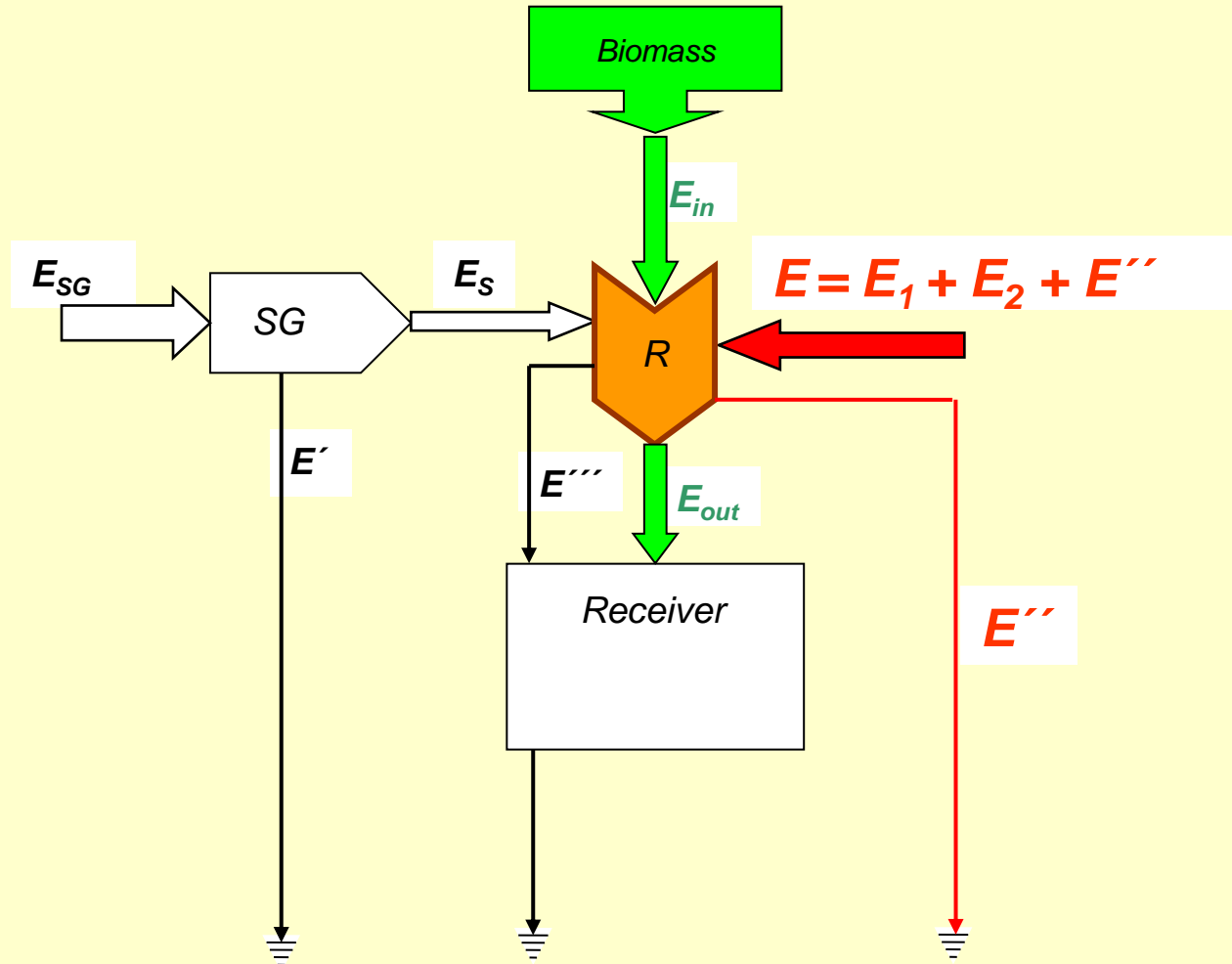
$$F = \frac{E_o}{E}$$

Required energy
Consumed energy

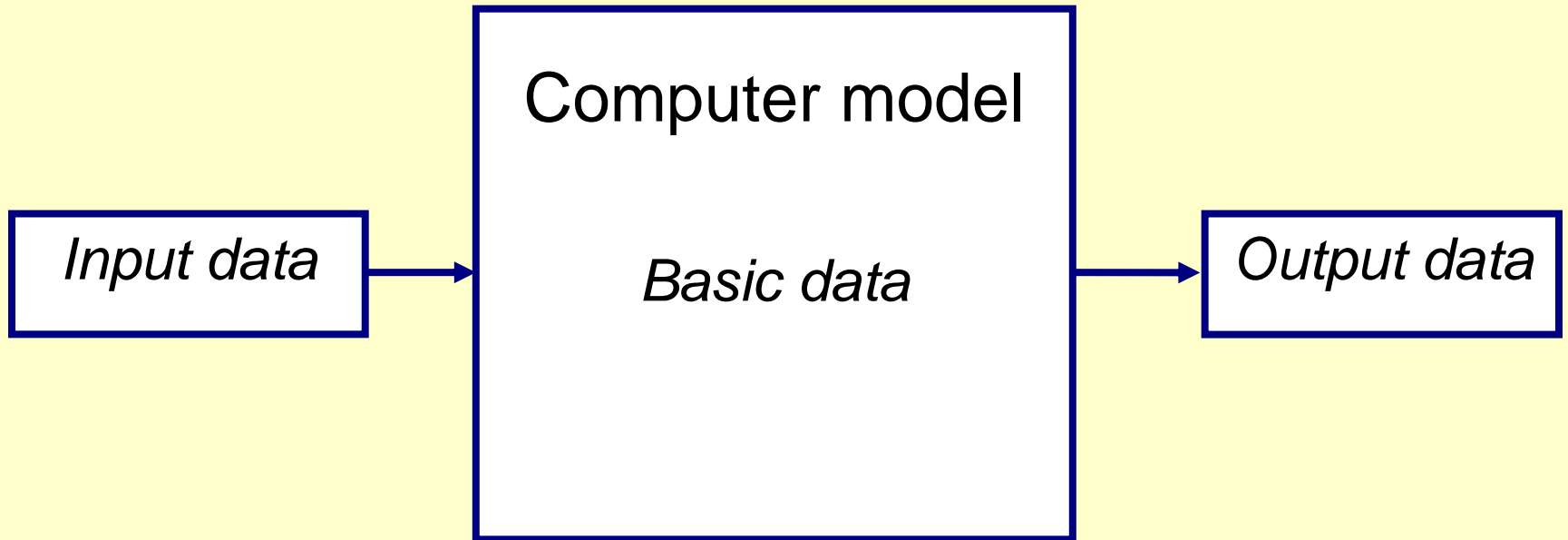
In units of biomass combustion energy E_c

$$F = \frac{E_o / E_c}{E / E_c} \quad \longrightarrow \quad \frac{E_c}{E} = \frac{F}{E_o / E_c}$$

Energy Flows



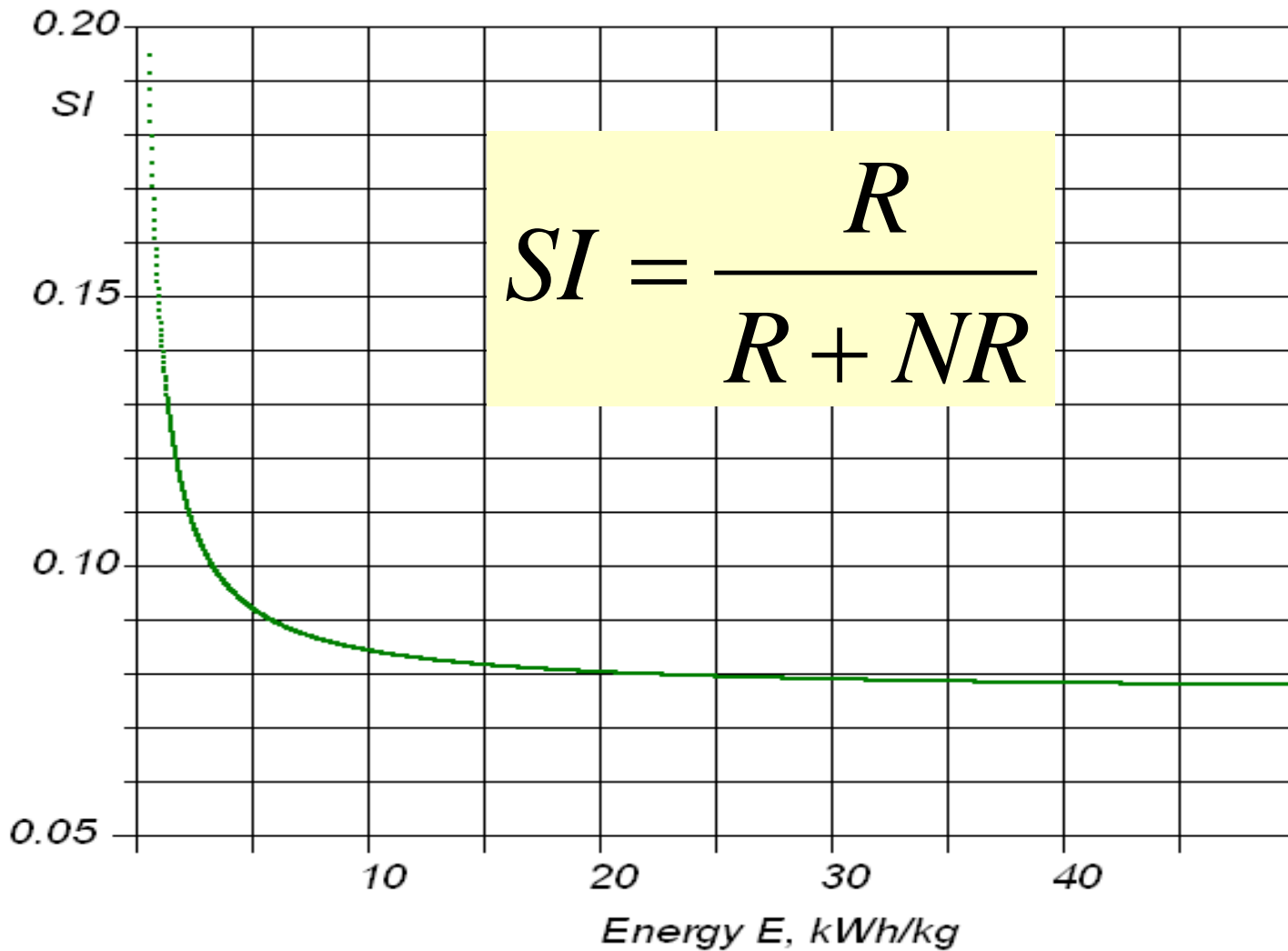
Modelling SE energy flows



Basic Data

Description	Value, kJ/kg K
Heat capacity of biomass	2.7
Heat capacity of water	4.19
Heat of water evaporation	2257
Enthalpy of steam at 60 bar, 100 °C	423
Enthalpy of steam at 60 bar, 250 °C	1085

Sustainability (for all biorafineries)



Energies and indicators

Description	Value
Non-renewable emergy (NR)	1088 MWh-sol
Renewable emergy (R)	89.6 MWh-sol
Conditionally renewable emergy (SR)	26 MWh-sol
Emergy yield (EY)	1203.6 MWh-sol/kg
Added emergy ratio (AER)	45.3
Sustainability index (SI)	0.096
Environmental load (L)	0.926

**When written in Chinese, the word
“crises” is
composed of two characters - one
represents **danger** and one
represents **opportunity****

危機



Questions?